

1 **Sustainable green extraction of anthocyanins and carotenoids using natural**
2 **deep eutectic solvents (NaDES): A review of recent developments**

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21 **Abstract**

22 Recently, deep eutectic solvents (DES) have been extensively researched as a more biocompatible
23 and efficient alternative to conventional solvents for extracting pigments from natural sources. The
24 extraction efficiency of DES extraction for the anthocyanin and carotenoid extraction can be
25 enhanced by microwave-assisted extraction (MAE) and/or ultrasound-assisted extraction (UAE)
26 techniques. Apart from the extraction efficiency, the toxicity recovery of the pigments and the
27 bioavailability are crucial for potential applications. A plethora of studies are presently examining
28 the extraction efficiency, toxicity, and recovery of pigments from various natural plant-based
29 matrices using DES. Nevertheless, a detailed review of the deep eutectic solvent extraction of
30 natural pigments has not been reported to date. Additionally, the toxicity, safety, and
31 bioavailability of the extracted pigments, and their future potentials are not thoroughly
32 documented. Therefore, this review is designed to understand the aforementioned concepts in
33 using DES for anthocyanin and carotenoid extraction.

34

35 **Keywords:** anthocyanins; carotenoids; deep eutectic solvents; natural deep eutectic solvent;
36 pigment extraction; green extraction.

37 **1. Introduction**

38 The history of pigments dates back to ancient Egyptians who used *Rubia cordifolia* for dyeing the
39 textile (Orna & Fontani, 2022). Since then the use of pigments has been explored in the food
40 industry, biomedical sciences, and cosmetic industry, and is well-studied for the prevention and
41 treatment of diseases. The exponential growth in these industries, over the years, has demanded
42 the production of pigments. According to Future Market Insights, the market value for the
43 production of synthetic pigments was USD 5,862.0 million and is anticipated to have a growth rate
44 of 4.5% by the year 2032, which accounts for USD 9,824.9 million (Future Market Insights, 2021).
45 However, the production of synthetic pigments is expected to grow by 76% while natural pigment
46 production is predicted to have a 24% fall (Rodríguez-Mena et al., 2022). The major factor that
47 affects the decline in natural pigment production is the instability of the natural pigments to light,
48 heat, oxygen, organic compounds, metal ions, and pH (Rodrigues et al., 2020; Shen et al., 2022).
49 Moreover, unlike synthetic pigments, significant amounts of natural pigments are required for the
50 production of equal color strength. Nevertheless, due to the obvious toxic effects associated with
51 synthetic pigments upon prolonged usage, natural pigments are gaining attraction in recent years
52 to partially or completely replace synthetic pigments (Di Salvo et al., 2023). As a result, many
53 studies are being explored to investigate the efficient extraction process and the chemical
54 intactness of the natural pigments.

55

56 The conventional extraction methods used in the extraction of natural pigments are simple, yet
57 provide poor extraction efficiency. Furthermore, the type of extraction solvents and the
58 temperature of extraction are two vital parameters that vastly affect extraction efficiency. The
59 increased amounts of extraction solvents required for efficient pigment extraction can lead to
60 toxicity, flammability, and non-biodegradability (Jacobsen et al., 2019). To overcome the

61 challenges in conventional extraction methods, innovative extraction techniques such as
62 microwave-assisted extraction, ultrasound-assisted extraction, pulse electric field, and superficial
63 extraction techniques are investigated (Rodríguez-Mena et al., 2022). Similarly, the use of neoteric
64 extraction solvents such as DES and its subclass NaDES are explored as a substitute for
65 conventional extraction solvents (Liu et al., 2019).

66
67 Considering the increased need for natural pigment and the efficient extraction process, this review
68 aims to comprehend the different extraction methods used for the recovery of anthocyanins and
69 carotenoids– with a major focus on DES/NaDES as green extraction solvents (**Figure 1**). Besides,
70 the toxicology and safety of the anthocyanins and carotenoids extracted using DES/NaDES were
71 discussed followed by their usage in the food industry and the future perspectives and limitations.

72

73 **2. Conventional and novel extraction methods of natural pigments**

74

75 The extraction of natural pigments from plants using conventional methods such as Soxhlet,
76 maceration, percolation, and solvent extraction methods have been widely studied (Lotfi et al.,
77 2015). These conventional methods are time-consuming, require large amounts of extraction
78 solvents, non-cost effective, and are mostly non-specific (Jacobsen et al., 2019). The choice of
79 organic solvents used in the extraction of pigments is dependent on the class of pigment. On one
80 hand, polar pigments like anthocyanins are extracted with ethanol, methanol, and water (Monrad
81 et al., 2010). On the other hand, non-polar pigments like β -carotene and lycopene, which are highly
82 lipophilic carotenoids require non-polar solvents like hexane and acetone. β -carotene and lycopene
83 lack polar functional groups due to the conjugated hydrocarbon structures (Saini & Keum, 2018).
84 These conventional solvents are toxic, highly volatile, flammable, and can negatively impact the

85 environment (Zainal-Abidin et al., 2017). Similarly, there have been reports of poor stability of
86 the pigment and extract obtained by conventional solvents (Martins et al., 2016). Hence, there is a
87 pivotal need to develop a suitable solvent that is stable, safe, and efficient (Z. Yu et al., 2022a).
88 Currently, significant progress has been made to overcome the challenges in extracting pigments.

89
90 Ionic liquids are one the most explored solvents for the extraction of pigments. ILs are synthesized
91 by various anions and organic cations. They have found useful applications in the extraction of
92 pigment, bioactive compounds, biomolecular research, pharmaceuticals, and organic synthesis
93 (Cao et al., 2018). A study by Murador et al. (2019) evaluated the extraction yield of carotenoid
94 from orange peel using ILs compared to conventional solvent. The carotenoids obtained from ILs
95 were more stable with higher antioxidant activity compared to conventional solvents like acetone.
96 However, ILs are highly priced, and hence utilizing ILs for the extraction of pigment is not a
97 feasible solution, especially at a larger scale (Abushammala & Mao, 2020). In addition, some
98 studies reported a high-level of toxicity and impaired biodegradability of ILs (Salam et al., 2016).
99 Due to the constraints associated with organic solvents and ILs, new alternative solvents are being
100 explored. These solvents are chosen based on their health and environmental toxicity,
101 biodegradability, cost, and extraction efficiency.

102
103 Deep eutectic solvent (DES), which was first synthesized by Abbott et al. (2004) is a new class of
104 solvent that is promising for pigment extraction. DESs are analogues to synthetic ILs and are
105 mostly obtained from various natural sources, which makes them suitable for the green extraction
106 of pigments. Mainly, plant metabolites and/or cellular constituents are extracted and mixed in
107 different proportions to obtain eutectic mixtures. Interestingly, each constituent of the eutectic
108 mixture has a higher melting point, however, when they are mixed together, the components will

109 melt at a much lower temperature (Dai et al., 2013). For example, in a DES that consists of choline
110 chloride and urea, the melting points of choline chloride and urea are 302 and 133 °C, respectively.
111 When these two components are mixed, the mixture melts at less than 60 °C while the freezing
112 point depression occurs at 12 °C this temperature is known as the “eutectic temperature” and the
113 mixture is known as the “eutectic mixture”. Since choline chloride and urea are obtained from
114 natural sources, these solvents are labelled as “natural deep eutectic solvent (NaDES)” (Ijardar et
115 al., 2022; Ling & Hadinoto, 2022). The possibility of these solvent mixtures melting at a much
116 lower temperature, than their melting points, is attributable to the intermolecular interaction
117 between the HBD and the HBA which expands the size of the NaDES complex and reduces the
118 electrostatic interactions consequently the energy required to melt the NaDES is reduced (Pan et
119 al., 2021). Depending on the nature of constituents, the DES can be classified into five types: Type
120 I (mixture of quaternary ammonium salt and metal chloride); Type II (mixture of quaternary
121 ammonium salt and hydrate of metal chloride); Type III (mixture of quaternary ammonium salt as
122 hydrogen bond acceptor (HBA) and amines, amides, carboxylic acids, alcohols, and sugars as
123 hydrogen bond donor (HBD) to form ionic NaDES); Type IV (mixture of metal chloride and any
124 HBD); and Type V (mixture of non-ionic HBD and HBA) (Choi et al., 2011). Nevertheless, type
125 III has been widely explored in recent years for its selectivity in extracting various components
126 and has been substantiated with less toxicity. In a type III eutectic system that consists of choline
127 chloride and urea, the choline chloride acts as HBA and urea acts as HBD. Through the
128 intermolecular hydrogen bond interactions, the lattice energy of the mixture decreases— requiring
129 a lower temperature to melt, resulting in a lower eutectic temperature. Figure 2 illustrates the
130 interaction in a eutectic mixture and the potential to selectively extract the pigments.

131

132 **3. Extraction of anthocyanins using DES/NaDES: influential factors**

133 Anthocyanins are a class of polyphenols mainly found in fruits, vegetables, and flowers. Due to
134 the substantial health benefits manifested by anthocyanins, these compounds are incorporated into
135 foods to be used as functional foods. Besides, anthocyanins are added to foods as natural colorants
136 replacing synthetic food colorants (Dai et al., 2016). In light of such facts, extracting anthocyanin,
137 from natural sources, using type III DES/NaDES has gained a lot of attention due to the
138 intermolecular interactions that can be formed between the hydroxyl and carbonyl groups of
139 anthocyanins with the eutectic mixture (Alrugaibah et al., 2021). The intermolecular interactions
140 are highly influenced by pH, polarity, viscosity, water as the co-solvent, and the solid-to-solvent
141 of the eutectic system. Furthermore, to enhance the extraction efficiency of anthocyanins,
142 integrative techniques such as microwave-assisted extraction (MAE) (Evitasari et al., 2022; Han
143 et al., 2023) and ultrasound-assisted extraction (UAE) (Jovanović et al., 2022; MacLean et al.,
144 2021; Thakur et al., 2022; Velásquez et al., 2021) are commonly used along with the DES. The
145 temperature and the duration of the treatment of these techniques greatly influence the degree of
146 anthocyanin extraction. Collectively, the nature of type III DES/NaDES and the mechanical
147 extraction techniques used significantly affect the extraction efficiency of anthocyanins. The
148 structure of some anthocyanins is depicted in **Figure 3** showing the variation in the functional
149 groups in their structure. The proceeding section will illustrate the effects of individual parameters
150 on the extraction efficiency of anthocyanins.

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153

154

155 **3.1 Effect of pH on DES/NaDES extraction of anthocyanins**

156

157 Depending on the pH, anthocyanins can exist in various forms. At acidic pH <4, pH 6-8, and pH
158 >8, anthocyanins exist as cation flavylum, quinoidal base, and chalcone, respectively (Bosiljkov
159 et al., 2017). Since these species differ in their functional groups, the interaction between the
160 anthocyanins and the DES will highly depend on the pH of the DES. The DES/NaDES that contain
161 organic acids have the potential to stabilise the flavynium ion because these acids can stabilize the
162 phenolic groups in C4', C5, and C7 (Dangles et al., 2018). In contrast, when alkaline groups such
163 as amide or amine are present as HBD in the DES/NaDES, the flavynium cation can be destabilized
164 which in turn reduces the extraction efficiency (Khoo et al., 2017; Bosiljkov et al., 2017). When
165 bilberry anthocyanin was extracted using choline chloride-lactic acid and choline chloride-urea,
166 the total anthocyanin content was 2.5 and 0.9 mg CGE/ g DW respectively (Jovanović et al., 2022).
167 The alkaline pH of choline chloride-urea causes the destabilization of anthocyanin resulting in
168 poor anthocyanin extraction. In terms of anthocyanins from Chilean berries (*Luma chequeen*), the
169 total anthocyanins were high in lactic acid-glucose DES (3.3 mg/g DW) compared to tartaric acid-
170 glycerol (0.8 mg/g DW) due to the comparative acidic pH of lactic acid-glucose (Velásquez et al.,
171 2021). Similarly, when the anthocyanin was extracted from black rice bran powder using various
172 DES, the highest and the lowest anthocyanin were obtained with lactic acid-fructose (32.5 mg/L)
173 and sucrose-fructose-glucose (7.5 mg/L), respectively (Thakur et al., 2022). Other studies have
174 also reported high yield of anthocyanins extracted from several plant sources using acid-based
175 DES such as perilla leaves (Han et al., 2023), wine lees (Bosiljkov et al., 2017), blackberry
176 (Zannou & Koca, 2022), grape skin (Iannone et al., 2021), blueberry (da Silva et al., 2020), and
177 mulberry (Guo et al., 2019). Thus, the anthocyanin extraction can be enhanced by using an acid-
178 based DES.

179

180 **3.2 Effect of DES/NaDES polarity on the extraction of anthocyanins**

181

182 Anthocyanins are polar compounds due to the rich hydroxyl and carbonyl groups. Hence, they
183 dissolve well in polar DES/NaDES due to polar-polar interactions. The raspberry anthocyanins
184 were extracted more in choline chloride-1,4-butanediol compared to choline chloride-glycerol,
185 choline chloride-glycol, and choline chloride-glucose, due to the high polarity of choline chloride-
186 1,4-butanediol (Xue et al., 2020). The extraction of black rice bran was favored in a lactic acid-
187 fructose eutectic mixture compared to a mixture that had sucrose-fructose-glucose (Thakur et al.,
188 2022). Various other studies with blackberry (Zannou & Koca, 2022), blueberry (da Silva et al.,
189 2020), and chokeberry (Jovanović et al., 2023) have also shown high extraction efficiency of
190 anthocyanins in highly polar DES. The increased polar-polar interactions are owed to the hydrogen
191 bonds that forms between anthocyanins and DES/NaDES– to enhance the extraction.

192

193 **3.3 Effect of DES/NaDES viscosity and water content on the extraction of anthocyanins**

194

195 The viscosity of the DES/NaDES plays an important role in the extraction and stabilization of the
196 anthocyanins. In this section, only the effect of viscosity on the extraction of anthocyanin will be
197 discussed and the stability will be discussed in the later section. When the viscosity of the
198 DES/NaDES is high, the molecular movement gets hampered making the solid-solvent interaction
199 less, thus resulting in less extraction efficiency (Han et al., 2023; Zannou & Koca, 2022). For
200 example, the bilberry extract showed high anthocyanin extraction in a choline chloride-lactic acid
201 mixture compared to choline chloride-citric acid, choline chloride-malic acid, and choline
202 chloride-tartaric acid (Jovanović et al., 2022) although lactic acid is a monoprotic acid. This

203 observation could be attributed to the higher viscosity of the NaDES consisting of di and tri-protic
204 acids. Airouywa et al., (2023) reported that higher molecular weight carboxylic acid-based NaDES
205 possess higher viscosity; in the study of physicochemical properties of carboxylic acids based-
206 NaDES, consisting of lactic acid, acetic acid, malic acid and citric acid as HBD while choline
207 chloride as HBA, the HDB with di and tri protic acids possess higher viscosity compared to the
208 monoprotic acids (acetic acid and lactic acids). The viscosity of choline chloride:lactic acid,
209 choline chloride:acetic acid, choline chloride:malic acid, and choline chloride: citric acid at 1:2
210 molar ratio were 20, 30, 6000, and 6800 cP, respectively. The high viscosity hinders the extraction
211 efficiency due to the suppressed mass transfer within the system. Similarly, raspberry
212 anthocyanins were extracted better in choline chloride-1,4-butanediol compared to other choline
213 chloride-based eutectic mixtures (Xue et al., 2020). In a study when the chokeberry was extracted
214 with hydroxypropyl- β -cyclodextrin in DES mixture, the extraction efficiency increased up to 3%
215 of hydroxypropyl- β -cyclodextrin and decreased with further increase of hydroxypropyl- β -
216 cyclodextrin. The initial increase could be due to the optimal “host-guest” interaction between
217 anthocyanin and cyclodextrin to form an inclusion complex and stabilize the encapsulated
218 anthocyanin. However, the decrease in anthocyanin extraction with increasing amount of
219 hydroxypropyl- β -cyclodextrin can be directly related to the increased viscosity of the medium,
220 which suppresses the anthocyanin extraction (Jovanović et al., 2023). Apart from these studies,
221 several other studies (da Silva et al., 2020; Han et al., 2023; Zannou et al., 2020) have also reported
222 a similar correlation between the viscosity and the extraction efficiency of anthocyanin.

223

224 Interestingly, when water is used as a co-solvent in a DES/NaDES mixture, the viscosity gets
225 altered, resulting in significant changes in extraction efficiency. In addition, the use of water as the
226 co-solvent increases the polarity of the DES/NaDES to increase the polar-polar interaction

227 between the DES/NaDES and anthocyanin (Vannuchi et al., 2022). Thus, the increased
228 anthocyanin extraction efficiency of water is attributed to the decrease in the viscosity and increase
229 in the polarity of the DES/NaDES. The addition of water reduces the viscosity of the DES/NaDES
230 through the loss of the DES/NaDES supramolecular structure (Lanjekar et al., 2021). The
231 reduction in viscosity favors high mass transfer and facilitates the extraction of anthocyanin.
232 However, adding too much of water can disrupt the supramolecular network of DES and hence
233 suppress the efficiency of extraction (Vannuchi et al., 2022). Extraction of anthocyanins from
234 perilla leaves showed an increase of anthocyanin extraction yield from 470 to 508 mg /100 g DW
235 when the water content was increased from 10 to 20%. However, when the water content was
236 further increased to 30, 40, and 50% there was a steady decline in the anthocyanin extraction yield
237 (Han et al., 2023). Mulberry anthocyanin extraction showed increased extraction yield when the
238 water content in DES/NaDES increased from 10 to 30%. Afterwards, the extraction yield
239 decreased as the water content increased to 40 and 50% (Guo et al., 2019). Although increasing
240 the water content can favor the polarity of the DES/NaDES and a further decrease in the viscosity
241 of the DES/NaDES mixture causes disruption in the molecular network among DES/NaDES,
242 anthocyanin, and water matrix, thus impeding the extraction efficiency by weakening the bond
243 between DES/NaDES and anthocyanin. Therefore, viscosity and the content of water play a crucial
244 role in anthocyanin extraction.

245

246 **3.4 Effect of solid-to-liquid ratio on the extraction of anthocyanins using DES/NaDES**

247

248 The solid-to-liquid ratio is another important factor that affects the extraction of anthocyanins. The
249 high amount of solvent aids mass transfer through a concentration gradient and provides a high
250 collision probability for the liquid to penetrate the plant cells (MacLean et al., 2021; Xue et al.,

251 2020). When the liquid penetrates the cell wall matrix the anthocyanins can be easily extracted
252 into the liquid due to the higher concentration gradient between solid and solvent. An increase in
253 anthocyanin extraction from bran rice was observed when the liquid-to-solid ratio was gradually
254 increased from 18.75 ml/g to 32.5 ml/g and no further increase was observed above 32.5 ml/g
255 (Thakur et al., 2022). Similarly, raspberry anthocyanin extraction increased from 1.04 to 1.25 mg/g
256 when the solid-to-liquid ratio was increased from 1:10 to 1:20, respectively. However, a further
257 increase in the solid-to-liquid ratio (1:25 and 1:30) did not show a significant increase in the yield
258 of anthocyanin (Xue et al., 2020). In contrast, purple perilla leaves the extraction yield of
259 anthocyanin had a statistically significant increase from 365 to 450 mg/100g DW when the solid-
260 to-liquid ratio increased from 1:4 to 1:10 (Han et al., 2023). These findings clearly suggest that the
261 solid-to-liquid ratio does not always proportionately increase the extraction efficiency of
262 anthocyanin and this could be attributed to the high content of liquid that can suppress the mass
263 transfer from the solid phase .

264
265 Not only the aforementioned factors but also the integrative techniques can impact the extraction
266 efficiency of anthocyanins. The ultrasound-assisted extraction (UAE) and microwave-assisted
267 extraction (MAE) are the two commonly used extraction techniques that are used in extracting
268 anthocyanins from various raw materials (Guo et al., 2019). Using UAE, the anthocyanin
269 extraction efficiency is increased through the acoustic waves, which will mechanically agitate the
270 plant cell walls to rupture and at the same time create acoustic cavitation in the solvent medium.
271 When the plant cell walls are ruptured, the anthocyanins become exposed to the DES/NaDES
272 hence making the extraction process efficient. In addition, when acoustic cavitation is created the
273 temperature in those regions increases and the viscosity decreases. The decreased viscosity
274 enhances the feasibility of the solvent to penetrate the plant cell walls and extract the anthocyanin

275 (Jovanović et al., 2023; Thakur et al., 2022). Thus, these two effects synergistically work to
276 enhance the anthocyanin extraction. Furthermore, in a UAE extraction method– the duration of the
277 treatment, temperature, and the amplitude of the ultrasounds impact the extraction of anthocyanin.
278 The Haskap berries showed maximum anthocyanin extraction when the ultrasound treatment was
279 provided for 10 min at 75 °C (MacLean et al., 2021). Similarly, for black rice bran, the maximum
280 anthocyanin extraction was achieved at 11.25 min at 21.31% amplitude of ultrasonication (Thakur
281 et al., 2022). When raspberry anthocyanins were extracted with UAE– the maximum anthocyanin
282 extraction was obtained at 210 W, 51 °C, and 32 min of power, temperature, and time, respectively
283 (Xue et al., 2020). Depending on the cell matrix, the UAE parameters can vary and therefore,
284 optimization studies have been carried out. Several other studies (Velásquez, Bustos, Montenegro,
285 and Giordano (2021); Han et al. (2023); Alrugaibah, Yagiz, and Gu (2021)) have also optimized
286 the extraction efficiency of anthocyanin from different sources.

287

288 MAE can be used as an alternative for UAE in anthocyanin extraction. The operating principle for
289 MAE to extract anthocyanin is based on the ability of the microwaves to create rotational motion
290 of the molecules, in a solid-liquid mixture, which can generate heat energy and accelerate the
291 anthocyanin extraction. Three main factors determine the extraction efficiency of anthocyanin
292 using microwave: microwave power, temperature, and time (Han et al., 2023). When purple perilla
293 leaves were subjected to microwave extraction for anthocyanin– the extraction yield increased
294 from 480 to 530 mg/100g DW at 40 and 60 °C, respectively while the microwave power was kept
295 constant at 400 W. However, further increases in temperature to 70 and 80 °C, drastically
296 decreased the anthocyanin yield. Similarly, when the microwave power was increased from 300
297 W to 400 W, the extraction yields steadily increased from 510 to 560 mg/100g DW and dropped
298 significantly with further increase in microwave power to 500 W. Interestingly, when the purple

329 peril leaves were exposed in the microwave for more than 30 min the anthocyanin extraction yield
330 significantly dropped (Han et al., 2023). In contrast, when Hibiscus anthocyanin was extracted
331 using MAE, the total anthocyanin content increased with increasing microwave power, from 250
332 to 600 W, and time (50 to 150 s) (Kurtulbaş et al., 2020). A different study showed that the
333 maximum anthocyanin yield for purple sweet potatoes was obtained at 270 W microwave power
334 for 193 s (Evitasari et al., 2022). These studies clearly show that depending on the species, time,
335 temperature, and microwave power– the MAE of anthocyanin can vary. Most likely, when the
336 microwave treatment is given at a significantly high temperature for a prolonged period of time–
337 the anthocyanins can degrade– since they are thermally labile molecules. In summary, both, UAE
338 and MAE can be used as potential integrative techniques to enhance the extraction of anthocyanins.
339 More research is needed in terms of using NaDES/DES in a pressurized liquid extraction process
340 to investigate the extraction efficiency and stability of the extracted anthocyanin.

341

342 **4. Stability of anthocyanins in DES/NaDES**

343

344 Unlike conventional methods, the DES/NaDES extracted anthocyanins have shown better thermal
345 and/or storage stability. This is mainly attributable to the extensive intermolecular interactions that
346 occur between the biomolecules, such as anthocyanins and the DES/NaDES. Such intermolecular
347 interactions can suppress the movement of anthocyanins-like molecules to prevent oxidative stress
348 and maintain better stability. Moreover, unlike conventional solvents, the DES/NaDES can form
349 strong acylation with anthocyanin, which makes it stable at higher temperatures (Ruesgas-Ramón
350 et al., 2017). In light of such fact, many studies have investigated the stability of the anthocyanins
351 extracted using DES/NaDES.

352

323 When Roselle (*Hibiscus sabdariffa* L.) anthocyanin extracted in DES was exposed to temperatures
324 40 to 100 °C for 20, 40, 60, 80, and 100 min the thermal degradation instantly occurred at 100 °C
325 due to the thermal instability of anthocyanin at very high temperatures. When these anthocyanins
326 were stored at 20, 4, and -20 °C, the anthocyanins gradually degraded with time, at all three storage
327 temperatures (Zannou et al., 2020). Similar observations were recorded with cyanidin of
328 *Catharanthus roseus*; at 20 °C, the degradation was rapid compared to the other two temperatures
329 (Yuntao Dai et al., 2016). The thermal stability of cyanidin from *C. roseus* was, also, studied by
330 measuring the half-lives ($t_{1/2}$). The cyanidin had a greater than four-fold increase of $t_{1/2}$, in lactic
331 acid: glucose DES/NaDES ($t_{1/2}$ = 277.3 min) compared to ethanol ($t_{1/2}$ = 72.2 min). The $t_{1/2}$ of
332 blueberry anthocyanins also showed a similar trend where in DES the $t_{1/2}$ was 141.6 min compared
333 to conventional organic solvent, where $t_{1/2}$ was 45.1 min (da Silva, Smaniotto, Costa, Baranzelli,
334 Muller, Somacal, Monteiro, Vizzotto, Rodrigues, Barcia, et al., 2021). The Brazilian berry
335 anthocyanins extracted with choline chloride: propylene glycol and choline chloride: malic acid
336 showed longer $t_{1/2}$ for choline chloride: malic acid ($t_{1/2}$ = 9.8 hr) as opposed to chloride: propylene
337 glycol ($t_{1/2}$ = 5.7 hr), at 60 °C. The affinity of malic acid to anthocyanin could be related to its
338 functional groups (Benvenuti et al., 2022). The same study also reported the anthocyanin stability
339 in terms of thermodynamic parameters: The enthalpy change (ΔH) for choline chloride: malic acid
340 was comparatively higher than choline chloride: propylene glycol. The significantly high ΔH is
341 due to the high activation energy (E_a) of choline chloride: malic acid (77.6 kJ/mol), which clearly
342 shows that the complex formed between anthocyanin and choline chloride: malic acid is stronger
343 and requires more energy to break the bonds for degradation. Interestingly, both, choline chloride:
344 malic acid and choline chloride: propylene glycol showed negative values for change in entropy
345 (ΔS) due to the highly ordered structure that forms between anthocyanin and the DES mixture.
346 The ΔS was highly negative for choline chloride: malic acid (ΔS at 60 °C was -42.7 J/mol)

347 compared to choline chloride: propylene glycol (ΔS at 60 °C was -75.6 J/mol) because of the
348 highly ordered structure that forms between anthocyanin and choline chloride:malic acid – due to
349 the intense intermolecular interactions. Overall, the anthocyanins extracted using DES have clearly
350 shown increased stability towards time-dependent degradation.

351

352 **5. Extraction of carotenoids using DES/NaDES**

353 Carotenoids are secondary metabolites found in the chloroplast or chromoplast of fruits,
354 vegetables, and microorganisms. Depending on the chemical structure, the carotenoids can be
355 classified as: (1) carotenes, the carotenoids that are composed of hydrocarbon (β -carotene,
356 lycopene); (2) xanthophyll, an oxygenated derivative of carotene (lutein, zeaxanthin, astaxanthin)
357 (Yu et al., 2022). The chemical structure of major carotenoids is illustrated in **Figure 4**. Since
358 these carotenoids are hydrophobic and lipophilic, the extraction is mostly facilitated by organic
359 solvents. However, recently, deep eutectic solvents have become promising solvents for extracting
360 carotenoids (Koutsoukos et al., 2019). The increased interest in carotenoid extraction using a green
361 solvent is owed to its substantial health benefits– which in turn is beneficial in, both, culinary,
362 food, and nutraceutical applications.

363

364 **5.1 Extraction of total carotenoids**

365

366 Carotenoids from *Lycium barbarum*, a berry with various medicinal properties, showed better
367 extraction yield when choline chloride and malonic acid were used at a 1:1 ratio. However with
368 increasing malonic acid concentration, the extraction efficiency declined. The optimal ratio of
369 choline chloride to malonic acid provided a favorable medium for carotenoids to be extracted.
370 Change in viscosity with increasing concentration of malonic acid would have been the major

371 reason for the decreased efficiency of carotenoids (Z. Yu et al., 2022b). A deep eutectic solvent
372 system with choline chloride and tartaric acid with ultrasound-assisted extraction and microwave-
373 assisted extraction showed better carotenoid extraction for apricot pulp. For example, the
374 carotenoid extraction with conventional solvent-coupled with UAE was 11.5 mg β -carotene/100g
375 DS, whereas with choline chloride-tartaric acid-UAE, the carotenoid extraction increased to 41.3
376 mg β -carotene/100g DS. Similarly, the carotenoid extraction was higher for choline chloride-
377 tartaric acid- MAE (26.7 mg astaxanthin/100g DS) compared to MAE with conventional solvents
378 (23.9 mg astaxanthin/100g DS). The increased carotenoids with DES could be attributable to the
379 strong intermolecular interaction between the carotenoids and the DES complex (Koutsoukos et
380 al., 2019). Orange peels are rich sources of carotenoids. When orange peel carotenoids were
381 extracted with various DES systems, menthol-camphor, menthol-eucalyptol, and lauric acid-
382 octanoic acid showed high yields. Compared to other DES systems used in this study, these three
383 solvents showed higher extraction due to the hydrophobicity. The higher extraction efficiency of
384 these three solvents is also reflected in the higher oxygen radical absorbance capacity assay
385 (ORAC)– mainly owed to the radical scavenging potential of these hydrophobic DES.
386 Nevertheless, in terms of storage stability, the carotenoids showed better stability with menthol-
387 eucalyptol, which could be mainly due to the higher thermal stability of menthol-eucalyptol
388 (Viñas-Ospino et al., 2023). Similarly, another study that screened 68-DES for carotenoid
389 extraction from orange peel showed better extraction with menthol: camphor coupled with UAE.
390 Interestingly, crude palm oil that has \approx 1% carotenoids showed the highest extraction yield with
391 menthol: lactic acid at 1:1.5 (212 ppm) compared to menthol: acetic acid at 1:1.5 (150 ppm) (A.
392 Viñas-Ospino et al., 2023b). In contrast to all these studies, buriti fruit (*Mauritia flexuosa*) did
393 show an increase in carotenoid when various choline chloride-based solvents (choline chloride
394 with ethylene glycol, glycerol, glycerol-xylitol, glycerol-PEG) were used for extraction. This

395 observation could be related to the weak interaction between buriti carotenoids and the DES
396 system due to their incompatible functional groups (Leite et al., 2021). In summary, high
397 carotenoid extraction is favored when the DES forms strong hydrophobic and/or lipophilic
398 interactions with different functional groups found in carotenoids.

399

400 **5.2 Extraction of carotenes**

401

402 Carotenes are a class of carotenoids that mainly include β -carotene and lycopene. The β -carotene
403 is mainly responsible for the orange, red, and orange-red color of fruits, vegetables, and flowers
404 (J. Yu et al., 2022). Due to the hydrophobicity of the β -carotene, the extraction efficiency can be
405 increased by using fatty acids such as HBD and HBA. In a study, where medium-chain fatty acids
406 and short alkyl-chain fatty acids were used as HBD and HBA, respectively, the extraction of β -
407 carotene increased when ternary DES/NaDES was used. In addition, with ternary DES, the highest
408 extraction efficiency of approximately $\approx 100\%$ was achieved when short (C_9) and medium chains
409 (C_{10} and C_{11}) were used at a 2:1:1 ratio. The tuning of fatty acid-based DES composition can
410 change the extraction efficiency of β -carotene by varying the degree of hydrophobic interactions
411 (Li et al., 2019). By the same token, the extraction of β -carotene from pumpkin showed high
412 extraction efficiency in a caprylic acid: capric acid eutectic mixture at 3:1. The higher extraction
413 efficiency of this eutectic mixture, compared to other mixtures used in this study, was due to the
414 increased solubility of the β -carotene in the eutectic mixture used. For example, caprylic acid:
415 capric acid and menthol: lauric acid mixture showed 200.8 and 97.2 $\mu\text{g/mL}$ of β -carotene
416 solubility, respectively and this was translated to high extraction efficiency in caprylic acid: capric
417 acid 96.7 $\mu\text{g/mL}$ and lowest extraction efficiency in menthol: lauric acid 81.4 $\mu\text{g/mL}$. Interestingly,
418 switching the polarity from hydrophobic to hydrophilic aided in recovering the extracted β -

419 carotene in the DES mixture. When water was added to the β -carotene extracted by DES a two-
420 phase separation was obtained due to the immiscibility of the fatty acid-based DES and water.
421 However, the addition of a mild base (NH_4OH) to this mixture resulted in a homogenous solution,
422 which eventually precipitated the β -carotene that was extracted in the DES which resulted in a
423 higher yield of recovery which was about $\approx 90\%$ (Stupar et al., 2021). Extraction of β -carotene
424 from tomato pomace using conventional solvents and eutectic mixture showed a statistically
425 significant difference in the extraction efficiency. The acetone: n-hexane (conventional solvent)
426 and ethyl acetate: ethyl lactate (eutectic mixture) showed extraction efficiency of 2117.6 and
427 1510.2 $\mu\text{g/g}$, respectively (Lazzarini et al., 2022). When β -carotene was extracted from *Phaffia*
428 *rhodozyma* yeast using ionic liquids and deep eutectic solvents, significantly high β -carotene was
429 obtained with choline chloride: butanoate at 1:2 (Mussagy et al., 2022). Overall, various studies
430 have proved the efficiency of DES in the extraction of β -carotene from different sources.

431
432 Lycopene, is another important carotenoid that is majorly found in tomatoes. One study with
433 different eutectic mixtures such as capric acid: menthol, capric acid: thymol, capric acid: lauric
434 acid, lauric acid: menthol, and lauric acid: thymol showed highest lycopene extraction of 7.5
435 mg/100g FW with capric acid: lauric acid at 1:2 ratio. The lowest yield 1.1 mg/100g FW was
436 obtained with capric acid: menthol at 1:2 ratio. This could be attributable to the density and the
437 flow behavior index of the eutectic mixtures. In the case of capric acid: menthol, the density was
438 slightly higher than capric acid: lauric acid, which was 0.989 and 0.986, respectively. This was
439 also translated to the high flow behavior index of capric acid: menthol (1.2), compared to capric
440 acid: lauric acid (1.0). Hence, less mass transfer in a relatively high-density eutectic mixture could
441 hinder lycopene extraction (Kyriakoudi et al., 2022). Tomato pomace, one of the by-products of
442 the tomato industry, showed high lycopene extraction, 1446.6 $\mu\text{g/g}$, in menthol: lactic acid (8:1)

443 eutectic system when it was integrated with UAE at 70 °C for 10 min at 120 mL/g solvent-to-solid
444 ratio (Celeste Lazzarini et al., 2022). Another study showed that the lycopene extracted using ethyl
445 acetate: ethyl lactate accounted for 27.4 µg/g (Silva et al., 2019). The significant difference in the
446 lycopene extract in these two studies can be related to the UAE that facilitated the lycopene
447 extraction. In a fatty acid-based eutectic mixture, the highest lycopene of 90% was obtained when
448 the eutectic mixture was composed of 1-nonaic acid: n-decanoic acid: undecanoic acid at a 2:1:1
449 ratio (Li et al., 2019). The studies reported on lycopene extraction from tomato and tomato by-
450 products have clearly shown that deep eutectic solvents are efficient solvent systems in extracting
451 lycopene.

452

453 **5.3 Extraction of xanthophyll**

454

455 To date, astaxanthin is the highly explored xanthophyll for eutectic extraction. The astaxanthin is
456 mainly found in microorganisms and also accumulates in the shells of crustaceans, which consume
457 microalgae (Rodrigues et al., 2020). Extraction of astaxanthin from crab shells using a terpene-
458 based eutectic mixture showed the extraction yield was comparable to Soxhlet method using
459 acetone and eutectic mixture of menthol-myristic acid at 8:1 ratio, treated at 60 °C for 24-hours
460 (Rodrigues et al., 2020). In contrast, the high astaxanthin extraction was obtained with menthol-
461 myristic acid at an 8:1 ratio for shrimp, mussels, and *Haematococcus pluvialis* (Rodrigues et al.,
462 2020), compared to the conventional acetone-based Soxhlet method. When astaxanthin was
463 extracted from shrimp shell waste to utilize in bioactive films the maximum yield of 69.08 µg/g of
464 astaxanthin was obtained using choline chloride: lactic acid mixture at 1:1.02 ratio. The microalgae
465 *H. pluvialis* treated with oleic acid-terpene (thymol, menthol, and geraniol) showed maximum
466 extraction efficiency in the oleic acid-geraniol eutectic mixture due to the increased hydrophobic

467 interaction with astaxanthin. However, the stability of the extracted astaxanthin was high in the
468 oleic acid-thymol mixture due to the enhanced free radical scavenging ability of thymol, compared
469 to menthol and geraniol (Rodrigues et al., 2020). Another study with *H. pluvialis* showed
470 maximum extraction with choline chloride-butanoate (Pitacco et al., 2022). Astaxanthin extraction
471 from Gazami crab (*Portunus trituberculatus*) with methyl triphenyl phosphonium bromide-
472 glycerin eutectic mixture at 1:4 ratio integrated with 65 W ultrasonic power for 90 min resulted in
473 39.37 µg/g of astaxanthin of *P. trituberculatus* waste (Lee & Row, 2016). Similarly, other studies
474 have also shown efficient extraction of astaxanthin using eutectic mixtures from Brazilian shrimp
475 (*Litopenaeus vannamei*) (Santos et al., 2021) and shrimp by-products (Chandra Roy et al., 2021;
476 Zhang et al., 2014). All these studies have shown that due to the hydrophobicity of astaxanthin,
477 the extraction efficiency is high in hydrophobic eutectic systems, such as fatty acid-terpene
478 eutectic mixture.

479

480 **6. Toxicology of common DES used in pigment extraction**

481

482 Deep eutectic solvents (DES) are considered “green solvents” and “solvents of the 21st century”
483 (Paiva et al., 2014). When the components of DES are obtained from natural sources, the DES
484 forms a subclass that is known as Natural Deep Eutectic Solvents (NaDES). Both DES and NaDES
485 are considered benign, less-toxic, biodegradable, and cost-effective (Hayyan et al., 2013; Wen et
486 al., 2015; Zhao et al., 2015). Thus, these solvents are currently replacing conventional organic
487 solvents and ionic liquids for respective applications. Nevertheless, the toxicity and safety of the
488 DES and NaDES are debatable to date. Thus, the following section will cover the cytotoxicity and
489 biodegradability (ecotoxicity) studies conducted on the common DES and NaDES that are used
490 for the extraction of anthocyanins and pigments.

491
492 The commonly used eutectic solvents for anthocyanins and pigments are mainly based on choline
493 chloride and terpene. The choline is a major precursor for the synthesis of cell membrane and its
494 salt form, choline chloride, is considered safe as well (Martínez et al., 2022). The terpenes are
495 secondary metabolites of plants and hence are GRAS. However, when the NaDES are synthesized
496 with other natural metabolites such as sugars (glucose, fructose), sugar alcohols (xylitol, maltitol),
497 organic acids (malonic acid, oxalic acid), amides (urea)– the degree of toxicity changes due to the
498 intermolecular interactions (Rodrigues et al., 2020). These interactions also translate to various
499 physicochemical properties that can dictate the toxicity of the compounds. Studies (Hayyan et al.,
500 2013; Radošević et al., 2018) have shown that NaDES are more toxic compared to their individual
501 components. For example, the individual components (choline chloride, glycerin, ethylene glycol,
502 triethylene glycol, and urea) showed no toxicity with *Bacillus subtilis*, *Staphylococcus aureus*,
503 *Escherichia coli*, and *Pseudomonas aeruginosa*, but they did exert significant toxicity when the
504 eutectic mixture was synthesized based on choline chloride (Radošević et al., 2018). Similarly,
505 when citric acid was treated on different gram-positive and gram-negative bacteria, the toxicity
506 was less but the citric acid in a eutectic mixture manifested high toxicity (Radošević et al., 2018).
507 These observations can be attributed to the: (1) increase in viscosity of DES and/or NaDES, which
508 can hinder the oxygen availability and hence cause oxidative stress; (2) penetration of the eutectic
509 mixture through the cell membranes, which in turn can cause destabilization of the cell membrane
510 matrix through “Hofmeister colloidal principle”; (3) change in the pH of the eutectic mixture,
511 which can disrupt the biochemical functions in the cells; (4) addition of water as the ternary
512 component in the eutectic mixture, which can not only change the supramolecular structure of the
513 eutectic mixture but also the interaction of the eutectic mixture with the cell surface (Lomba et al.,

514 2021; Radošević et al., 2018; Sanchez-Fernandez et al., 2021). Due to these reasons, the
515 DES/NaDES have shown varying degrees of cytotoxicity and ecotoxicity.

516

517 The cytotoxicity quantified by EC₅₀ values showed that the choline chloride-oxalic acid had
518 significantly high toxicity for HeLa and MCF-7 cells and these were quantified as 2.48 mM and
519 4.19 mM, respectively. In addition, the same study showed that the choline chloride-urea was toxic
520 to MCF-7 cells and not to HeLa or HEK293T cells (Hayyan et al., 2013). The citric acid-trehalose
521 eutectic mixture at 12.24 μM concentration– a potential eutectic system for anthocyanins and/or
522 carotenoids, showed no cytotoxic effects on Zebrafish (Ferreira et al., 2022). Interestingly, when
523 choline chloride, tetramethylammonium chloride, and tetrabutylammonium chloride-based
524 eutectic systems were studied on human skin cells (HaCaT) and tumor melanocytes (MNT-1), the
525 cell viability dramatically decreased with increasing concentration of the eutectic mixture
526 (Macário et al., 2019). Especially with tetrabutylammonium chloride-urea mixture on HaCaT cells,
527 the decrease was significant compared to tetrabutylammonium chloride-hexanoic acid, butanoic
528 acid, 1-propanol, and ethylene glycol. In contrast, for MNT-1 cells, significant cell viability was
529 seen with tetrabutylammonium chloride-1-propanol. The selectivity of the eutectic mixture in
530 terms of decreasing the cell viability could be translated to the potential aggregation that can be
531 caused between the cell membrane and the eutectic solvent, which suppressed the tolerance of
532 cells for survival (Macário et al., 2019). The terpene-based eutectic solvents that are commonly
533 used for carotenoid extraction have shown varying degrees of cytotoxicity with Caco-2 cells. For
534 example, the astaxanthin extracted from crab shells with terpenes (perillyl alcohol, camphor,
535 menthol, eucalyptol) and myristic acid showed EC₅₀ between 0.5 to 1.1 mg/mL against Caco-2
536 cells. Similarly, shrimp shells, mussels, and *H. pluvialis* extracted with DES comprising of
537 menthol: myristic acid showed EC₅₀ of 1.5, 1.8, and 3.3 mg/mL against Caco-2 cells, respectively

538 (Rodrigues et al., 2020). Strikingly, another study with mice exposed to a choline chloride-urea
539 eutectic mixture showed cytotoxicity due to the elevated levels of ammonium which caused
540 oxidative stress due to oxygen and nitrogen (Jung et al., 2021). All the aforementioned studies
541 show that the varying degree of cytotoxicity depends not only on the nature of the eutectic mixture
542 but also on the type of cell lines used to study the cytotoxicity.

543

544 While cytotoxicity measures the protection of human health, ecotoxicity is imperative to monitor
545 environmental protection when using chemical solvents. In light of such fact, eutectic solvents are
546 also studied for ecotoxicity in both terrestrial and aquatic systems followed by their potential to
547 biodegrade. A concentration of 0.001 M of the citric acid-trehalose eutectic system was introduced
548 to water containing Zebrafish. The fish showed no toxicity when exposed to such an aquatic
549 environment (Ferreira et al., 2022). When different choline chloride and choline acetate-based
550 eutectic solvents with acetamide, urea, glycerol, and ethylene glycol at 0.01 M were introduced in
551 the freshwater ecosystem, the survival times of hydra was highly dependent on the nature of the
552 eutectic mixture (Wen et al., 2015). Overall, the survival time was higher for the choline acetate-
553 based eutectic solvent, compared to the choline chloride-based mixture; higher survival time (12
554 hours) were seen for choline acetate-acetamide and choline acetate-urea. However, the negative
555 growth of the tentacles in hydra occurred within a few hours— demonstrating the toxicity from the
556 eutectic mixture. The ecotoxicity studied on *Aliivibrio fischeri*, which is a model animal used to
557 study aquatic toxicity due to its luminescence effect, showed that all the eutectic mixtures (choline
558 chloride, tetramethylammonium chloride, tetrabutylammonium) showed ecotoxicity due to the
559 ability of these eutectic mixtures to penetrate the cells, mainly the cytoplasm, and cause disruptions
560 in the cellular process (Giner et al., 2020). In terms of the terrestrial system, the toxicity of the
561 eutectic mixture was studied based on the root growth of *Allium sativum*. Compared to control

562 samples (4.5 cm), all the other eutectic systems and their individual components showed truncated
563 growth of the roots. Mainly, the choline chloride-ethylene glycol had the lowest growth, compared
564 to others. In addition, the root tip cells were deformed, irrespective of the nature of the eutectic
565 solvent (Wen et al., 2015). Similar observations were also reported for *Triticum aestivum* species
566 (Nejrrotti et al., 2022). These observations could be supported by the fact that eutectic mixtures–
567 due to their strong intermolecular interactions– translated from the supramolecular structure, can
568 cross the cell surfaces and penetrate the subcellular levels to disrupt and/or attenuate the cell
569 growth. The biodegradability of the choline chloride and choline acetate studied against sodium
570 benzoate showed significantly lower biodegradability. The biodegradability over 14 days for
571 sodium benzoate, choline chloride-urea, and choline acetate-urea were 90, 78, and 40%,
572 respectively and the lowest biodegradability (25%) was observed for choline chloride-ethylene
573 glycol. Furthermore, the choline chloride-based eutectic mixture was more biodegradable than the
574 choline acetate-based eutectic mixtures, which could be due to the different degradation
575 mechanisms carried out by different soil microorganisms (Wen et al., 2015). In summary, the
576 ecotoxicity studies have shown that the eutectic mixtures are toxic to a certain extent for, both,
577 aquatic and terrestrial systems and show considerable amounts of biodegradability– although these
578 mixtures cannot be labelled as “readily biodegradable”.

579

580 **7. Bioavailability of pigments extracted using DES**

581

582 DES possess high bioavailability, bio-accessibility, and bio-stability due to the strong hydrogen
583 bonding network that is formed between DES and the bioactive compounds. However, only a few
584 studies on the bioavailability of the pigments extracted with DES have been reported. A study by
585 Zannou et al. (2022) reported the high bioaccessibility and bio-stability of anthocyanin extracted

586 with choline chloride: glycerol, by simulating the in vitro gastrointestinal model to mimic the
587 physiological in vivo digestion. The anthocyanin investigated, in this study, were cyanidin-3-
588 glucoside, cyanidin-3-rutinoside, pelargonidin-3-glucoside, and cyanin chloride and the
589 bioavailability of these anthocyanins accounted for 71.9 ± 0.5 , 77.3 ± 0.6 , 80.2 ± 0.7 , and $91.0 \pm$
590 1.0% , respectively. In general, the high pH in the intestinal environment biotransforms
591 anthocyanin by reducing its bioavailability. However, in this study, the bioavailability of the
592 anthocyanins was 70 to 90% and this is attributable to the ability of the choline chloride-glycerol
593 to protect the functional groups of anthocyanin; the extensive hydrogen bond network between the
594 DES (choline chloride-glycerol) and the anthocyanin (cyanidin-3-glucoside, cyanidin-3-
595 rutinoside, pelargonidin-3-glucoside, and cyanin chloride) prevents the biotransformation at
596 alkaline pH. In a different study, the bioavailability of blueberry anthocyanin in rats was compared
597 between DES (choline chloride-glycerol-citric acid) and organic solvent (methanol-water-formic
598 acid). When an equal amount of anthocyanin extracted from DES and organic solvent was
599 administered to the rats, the bioavailability of anthocyanin was 140% more in DES-based
600 anthocyanin, compared to organic solvent-based anthocyanin (da Silva et al., 2021). In addition,
601 the DES-extracted anthocyanin showed a biphasic profile in the gastrointestinal absorption
602 confirming the intactness of anthocyanin– when DES is used as the extraction solvent. Therefore,
603 the in vitro and in vivo digestion studies have shed some light on the bioavailability, bio-
604 accessibility, and bio-stability of the DES-extracted pigments. It is expected that more research in
605 this direction will unfold in the coming years to provide a better understanding of the
606 bioaccessibility and bioavailability of the NaDES-based anthocyanin extracts.

607

608

609

610 **8. Recovery of anthocyanin and carotenoid from DES/NaDES**

611 The recovery of carotenoid and anthocyanins from DES/NaDES is a challenging process because
612 these solvents possess low vapor pressure and can form strong molecular interactions between the
613 extracted compounds of interest, making the recovery process tasking. Several methods have been
614 described for removing target compounds from DES/NaDES which include, (1) liquid-liquid
615 extraction by including additional solvents, (2) antisolvent by addition of a solvent with different
616 polarity from the extraction solvent (3) solid phase extraction by using high-adsorbent resin and
617 chromatography (Grillo et al., 2020). de Souza et al. (2023) recovered 100% of the grape pomace
618 anthocyanins from DES using solid-phase extraction with a high-adsorbent resins. The resin can
619 also be reused from 1-8 cycles with an average recovery of $96\pm 1\%$ of grape pomace anthocyanin.
620 While the recycle yield of DES was $96\pm 1\%$ at the first recycle. Similarly, Panić et al., (2019)
621 reported the recovery of anthocyanins from grape pomace from NaDES using the solid-phase
622 extraction with macroporous resin. A total of 70.34% anthocyanins were recovered and 94.78%
623 NaDES recovered. In the recovery of anthocyanins from blueberry peel extract using absorption
624 chromatography and macroporous resin reported by Grillo et al., (2020). The results revealed that
625 the recovery of anthocyanins and NaDES were 72.55 and 79.48%, respectively. Furthermore, the
626 recovery of carotenoid from pumpkins using switchable NaDES was reported by Stupar et al.,
627 (2021). It was proposed that the possibility of separating carotenoids from hydrophobic NaDES
628 was based on the potential of the NaDES to switch its polarity by the addition of water and a weak
629 base to precipitate the carotenoid from the carotenoid NaDES-based extract. β -carotene was the
630 major carotenoid precipitate followed by β -cryptoxanthin with a total recovery of 52.25 and
631 38.04%, respectively. The possibility of recovery of anthocyanins and carotenoids from
632 DES/NaDES and the ability to reuse the DES and other materials like the microporous resin makes
633 the entire process economical and sustainable.

634 **9. Future perspectives and current limitations of DES in anthocyanin and carotenoid**
635 **extraction**

636

637 Over the past decade, DES and NaDES have gradually replacing conventional solvents for
638 extracting bioactive compounds. In alignment with such change, the extraction of anthocyanins
639 and carotenoids– which have significant applications in food and nutraceutical industries has
640 become a focus of attention.

641

642 One of the major challenges in using eutectic mixtures is to enhance the extraction efficiency and
643 recover the extracted component within a short period of time. In-situ preparation of the eutectic
644 mixtures and switchable eutectic solvents are investigated for the enhanced purification,
645 separation, rapid extraction, and recovery of eutectic mixture (Ahmadi et al., 2023; Stupar et al.,
646 2021; Zhang et al., 2023). In-situ preparation of eutectic mixtures is robust, compared to the
647 traditional eutectic mixture preparation; traditional preparation of eutectic mixture involves either
648 heating the eutectic mixture to a higher temperature for a longer period of time or freeze drying
649 the components in the eutectic mixture over few days. In contrast, an in-situ formation involves
650 the simultaneous complex formation of HBA and HBD in the sample mixture, where the HBA-
651 HBD complex can instantly bind to the components for rapid extraction (Ahmadi et al., 2023; Niu
652 et al., 2023). In terms of switchable eutectic solvents, these employ the changes in pH, temperature,
653 polarity, conductivity, density, and solubility. The flexibility to tailor the solvent system during
654 the extraction process makes eutectic solvents a versatile mixture (Zhang et al., 2023). The use of
655 a switchable solvent by changing the polarity has shown the efficient recovery of β -carotene from
656 pumpkin seeds (Stupar et al., 2021). In addition, switching the polarity to fractionate the biomasses

657 has also emerged in recent years. Although the switchable eutectic solvents are promising, the
658 research in this area is yet to be explored.

659
660 A recent investigation into DES/NaDES has revealed new findings in the field of biocatalysis. The
661 eutectics can act as, both, solvent and substrate (2-in-1) to increase the atomic efficiency of the
662 biocatalytic process (Pätzold et al., 2019). One such highly explored biocatalytic system is lipase-
663 based biotransformation– driven by the stereoselectivity of the DES/NaDES. Such an approach
664 can be translated to pigment extractions because mostly the first step of pigment extraction
665 involves an enzymatic reaction to disintegrate the pigments from the plant cell wall (Mićekus et
666 al., 2019). Under such circumstances, the Des/NaDES can be used as a co-solvent and substrate to
667 increase the efficiency of pigment extraction. Nevertheless, the molecular insights of such
668 transformations are yet to be explored.

669
670 Interestingly, the use of eutectic solvents for extraction in various applications involves optimizing
671 eutectic mixtures based on their molar ratio, solid-to-solvent ratio, pH, and thermal stability.
672 However, the process of screening eutectic solvents is time-consuming and involves significant
673 costs. Therefore, a recent advance in such area is the use of a Conductor-like Screening Model for
674 Real Solvents (COSMO-RS) to identify the best solvent for enhanced and rapid extraction of
675 bioactive compounds (Hayyan et al., 2016; Panić et al., 2021). Although the concept of COSMO-
676 RS is not new, the use of this software for eutectic solvent extraction can be considered relatively
677 new. In two recent studies, the eutectic solvents to extract bioactive components from blueberry
678 (da Silva, Smaniotto, Costa, Baranzelli, Muller, Somacal, Monteiro, Vizzotto, Rodrigues, &
679 Barcia, 2021) and grape pomace (Panić et al., 2021) were studied using COSMO-RS. Unlike
680 manual screening, the use of this computational model aided in screening multiple solvents to find

681 the suitable solvent for enhanced extraction. This technique can also be further extended to create
682 ready-to-use eutectic solvents, which facilitates the selection of an eutectic mixture to extract the
683 bioactive component of interest. Considering the aforementioned recent advances in extracting
684 bioactive components using eutectic mixtures, it is clear that the eutectic solvents are promising
685 for the extraction of anthocyanins and carotenoids.

686

687 **Conflict of interest**

688 All authors declare no conflicts of interest. For the purpose of open access, the author, Ali Ali
689 Redha, has applied a ‘Creative Commons Attribution (CC BY) licence to any Author Accepted
690 Manuscript version arising’.

691

692 **Author contribution**

693 Jennifer Osamede Airouyuwal: Writing - original draft, Revising the manuscript, data compilation

694 Nilushni Sivapragasam: Writing - original draft, Revising the manuscript, data compilation

695 Ali Ali Redha: Visualization, Writing - review & editing, data compilation, designing figures.

696 Sajid Maqsood: Conceptualization, Writing - review & editing, Project administration,

697 Supervision.

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1013 **List of tables**

1014 Table 1: Summary of studies on anthocyanin extraction from natural sources using DES/ NaDES
1015 and the extraction parameters used.

1016 Table 2: Summary of studies on carotenoid extraction from natural sources using DES/ NaDES
1017 and the extraction parameters used.

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1032 Table 1: Summary of studies on anthocyanin extraction from natural sources using DES/ NaDES
 1033 and the extraction parameters used.

Natural sources	Extracting solvent composition	Extraction method	Extraction yield of anthocyanin	Reference
Bilberry (<i>Vaccinium myrtillus</i> L.)	Choline chloride: sorbitol (1:1)	UAE	2.0 mg CGE/g DW	Jovanović et al. (2022)
Chilean berries (<i>Luma chequena</i>)	Lactic acid: glucose (8:1)	UAE	3.3 mg CGE/g DW	Velásquez, Bustos, Montenegro, and Giordano (2021)
Black rice (<i>Chakhao ambu</i>) bran	Lactic acid: fructose (1:1)	UAE	32.2 mg/L	Thakur, Gupta, Dhar, Deha, and Das (2022)
Haskap berry (<i>Lonicera caerulea</i> L.)	Citric acid: maltose (1:1)	UAE	21.2 mg/g DW	MacLean, Silva, Jiao, and Brooks (2021)
Perilla leaves	Choline chloride: ethylene glycol: lactic acid (1:1:1)	MUAE	6.2 mg/g DW	Han et al. (2023)
Cranberry (<i>Vaccinium macrocarpon</i>) pomace	Lactic acid: glucose (5:1)	UAE	1.6 mg/g DW	Alrugaibah, Yagiz, and Gu (2021)

Wine lees	Choline chloride: malic acid (1:1)	UAE	5.5 mg/g DW	Bosiljkov et al. (2017)
Purple sweet potato (<i>Ipomoea batatas</i> L.)	Citric acid: ethylene glycol (1:1)	MAE	311.6 mg/L	Evitasari, Rofiqoh, Damayanti, and Chusna (2022)
Jussara (<i>Euterpe edulis</i>) fruit pulp	Choline chloride: xylitol (1:1)	UAE	14.9 mg/g DW	Vannuchi, Braga, and De Rosso (2022)
Blackberry (<i>Rubus</i> spp)	Choline chloride: acetic acid (1:2)	UAE	1.2 mg CGE/g DW	Zannou and Koca (2022)
Grape (<i>Vitis vinifera</i>) skin	Citric acid: maltose (4:1)	UAE	42.0 mg/g DW	Jeong et al. (2015)
Mulberry (<i>Fructus Mori</i>)	Choline chloride: citric acid: glucose (1:1:1)	HSH-CBE	6.1 mg/g DW	Guo et al. (2019)
Blueberry (<i>Vaccinium</i> spp)	Choline chloride: glycerol: citric acid (0.5:2:0.5)	Heating in boiling water bath	3.6 mg CGE/g	da Silva et al. (2020)
Chokeberry (<i>Aronia melanocarpa</i>)	Choline chloride: lactic acid (1:2)	UAE	6.0 mg CGE/g DW	Jovanović et al. (2023)
Raspberry (<i>Rubus idaeus</i> L.)	Choline chloride: 1,4-butanediol (1:3)	UAE	1.4 mg/g DW	Xue, Tan, Li, Tang, and Cai (2020)

Brazilian berry (<i>Myrciaria cauliflora</i>)	Choline chloride: malic acid (1:1)	PLE	62.9%	Benvenuti, Zielinski, and Ferreira (2022)
Roselle (<i>Hibiscus sabdariffa</i> L.)	Sodium acetate: formic acid (1:2)	UAE	10.6 mg D3S/g DW	Zannou, Koca, Aldawoud, and Galanakis (2020)
<i>Catharanthus roseus</i>	Lactic acid: glucose & Choline chloride:1,2 propanediol	UAE	Not specified	Dai, Rozema, Verpoorte, and Choi (2016)
Roselle (<i>Hibiscus sabdariffa</i> L.)	Citric acid: ethylene glycol (4:1)	MAE	3.0 mg C3G/g DW	Kurtulbaş, Pekel, Bilgin, Makris, and Şahin (2020)

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1035 Abbreviations: CGE: cyanidin-3-O-glucoside equivalents, D3G: delphinidin-3-sambubioside
1036 equivalents, UAE: Ultrasound-Assisted extraction, MAE: Microwave-Assisted Extraction,
1037 MUAE: Microwave-Ultrasound-Assisted Extraction, PLE: Pressurized Liquid Extraction, HSH-
1038 CBE: High-speed homogenization and Cavitation-burst extraction.

1039 Table 2: Summary of studies on carotenoid extraction from natural sources using DES/ NaDES
 1040 and the extraction parameters used.

Natural sources	Extracting solvent composition	Extraction method	Extraction yield of pigments	Reference
Total Carotenoids				
<i>Lycium barbarum</i>	Choline chloride: malonic acid (1:1)	UAE	Peak area: Zeaxanthin (34,000) Zeaxanthin dipalmitate (118,00000)	Yu et al. (2022)
Shrimp head	Choline chloride: tartaric acid (2:1)	MAE	26.7 (mg astaxanthin/100 g DS)	Koutsoukos, Tsiaka, Tzani, Zoumpoulakis, and Detsi (2019)
Apricot pulp	Choline chloride: tartaric acid (2:1)	MAE	76.1 (mg of β -carotene/100 g DS)	Koutsoukos et al. (2019)
Buriti fruit (<i>Mauritia flexuosa</i> L.)	Choline chloride-based DES as co-solvent	Conventional extraction	Buriti pulp: 1006 (mg/100 g DW) Buriti peel: 1043 mg/100 g DW)	Leite et al. (2021)
Orange peel	Menthol: Eucalyptol (1:1)	Homogenization and stirring	150 (mg/ 100 g FW)	Viñas-Ospino, Panić, Bagović, et al. (2023)
Carotene (β-carotene and lycopene)				
<i>Phaffia rhodozyma</i>	Choline chloride: butanoate (1:2)	Stirring, centrifugation, and filtration	45% yield β -carotene	Mussagy et al. (2022)
Fruit juices (watermelon, grape, tomato, guava)	Fatty acid: C9:C10:C11 (2:1:1)	Centrifugation and filtration	>50% yield of β -carotene and lycopene	(Li, Zhao, Tian, Yang, & Li, 2019)
Pumpkin	Fatty acid: C8:C10 (3:1)	UAE	151.4 (μ g/ mL β -carotene)	Stupar et al. (2021)
Tomato pomace	Ethyl acetate: ethyl lactate (30:70 v/v)	Stirring, centrifugation, and filtration	3950.1 (μ g/g β -carotene) and 75.9 (μ g/g lycopene)	Lazzarini et al. (2022)
Xanthophyll (astaxanthin)				
<i>Haematococcus pluvialis</i>	Thymol: oleic acid (1:1)	Stirring, centrifugation	60% (yield in 6 hr)	Pitacco et al. (2022)

Shrimp by-products	Choline chloride:1,2-butanediol (1:2)	UAE	146 (µg/g)	Zhang, Tang, and Row (2014)
Shrimp residue	Choline chloride: glycerol (1:2)	UAE	32.7 (µg/g)	Santos et al. (2021)
<i>Portunus trituberculatus</i> waste	Methyl triphenyl phosphonium bromide:1,2-butanediol (1:4)	UAE	47.3 (µg/g)	(Lee & Row, 2016)
Shrimp waste	Choline chloride: lactic acid (1:2)	UAE	60.1 (µg/g)	(Chandra Roy et al., 2021)
<i>Phaffia rhodozyma</i>	Choline chloride: butanoate (1:2)	Stirring, centrifugation, and filtration	≈ 50% yield	(Mussagy et al., 2022)
Brown crab shell	Menthol: myristic acid (8:1)	Stirring and centrifugation	9.5 µg/g	(Rodrigues et al., 2020)

1041 Abbreviations: UAE: Ultrasound-Assisted extraction, MAE: Microwave-Assisted Extraction.

1042 **List of figures**

1043 **Graphical abstract**

1044 **Figure 1:** Schematic diagram of sources, extraction, and application of anthocyanins and
 1045 carotenoids (created using BioRender.com).

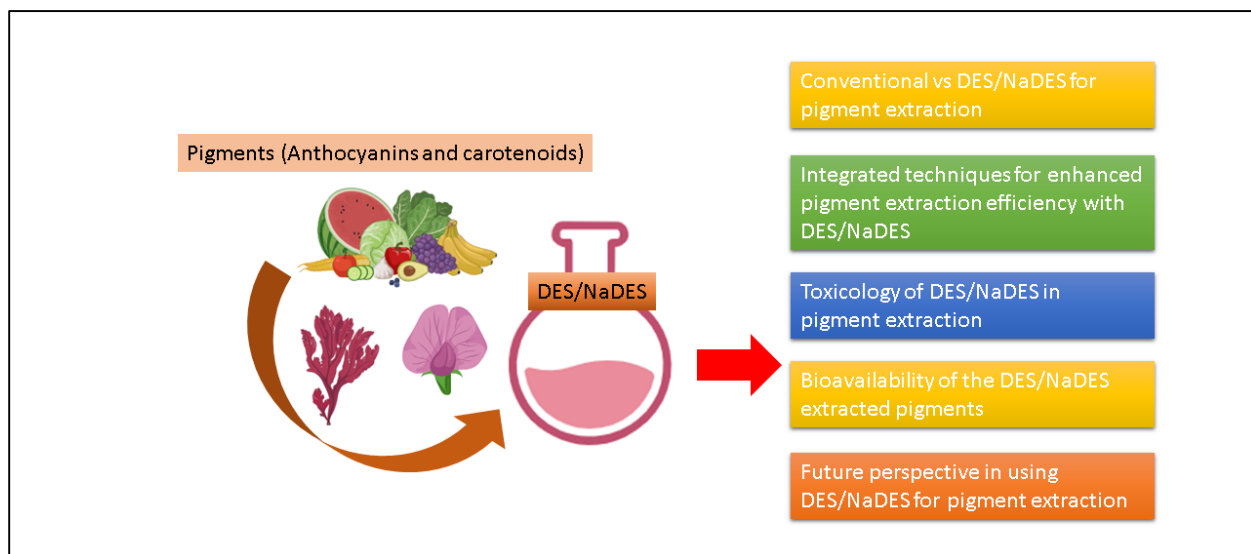
1046 **Figure 2:** Interaction of eutectic mixture and the enhanced selectivity towards pigment extraction
 1047 (created using BioRender.com).

1048 **Figure 3:** Chemical structure of selected anthocyanins with different functional groups and their
 1049 sources (created using BioRender.com).

1050 **Figure 4:** Chemical structure of major carotenoids.

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1052 **Figures**

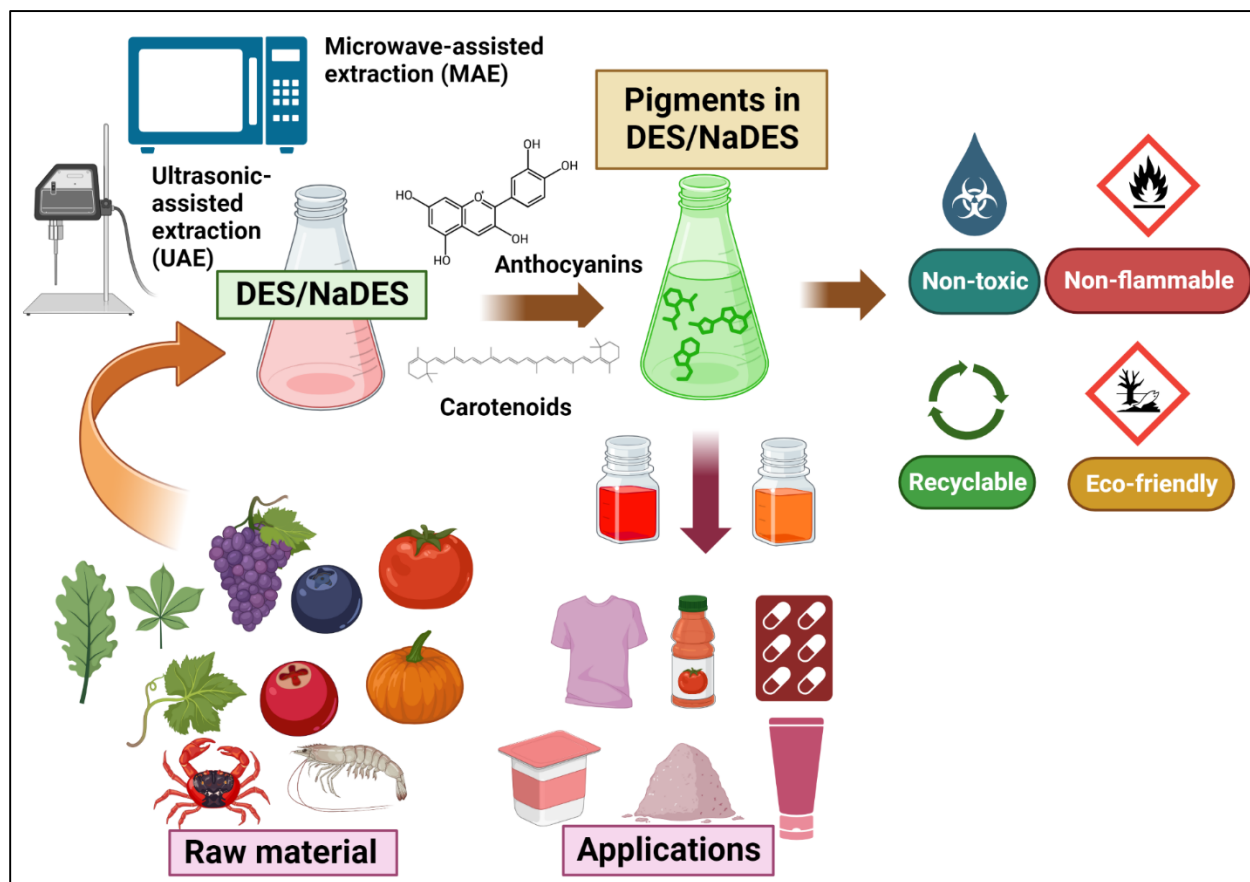


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1054 **Graphical abstract**

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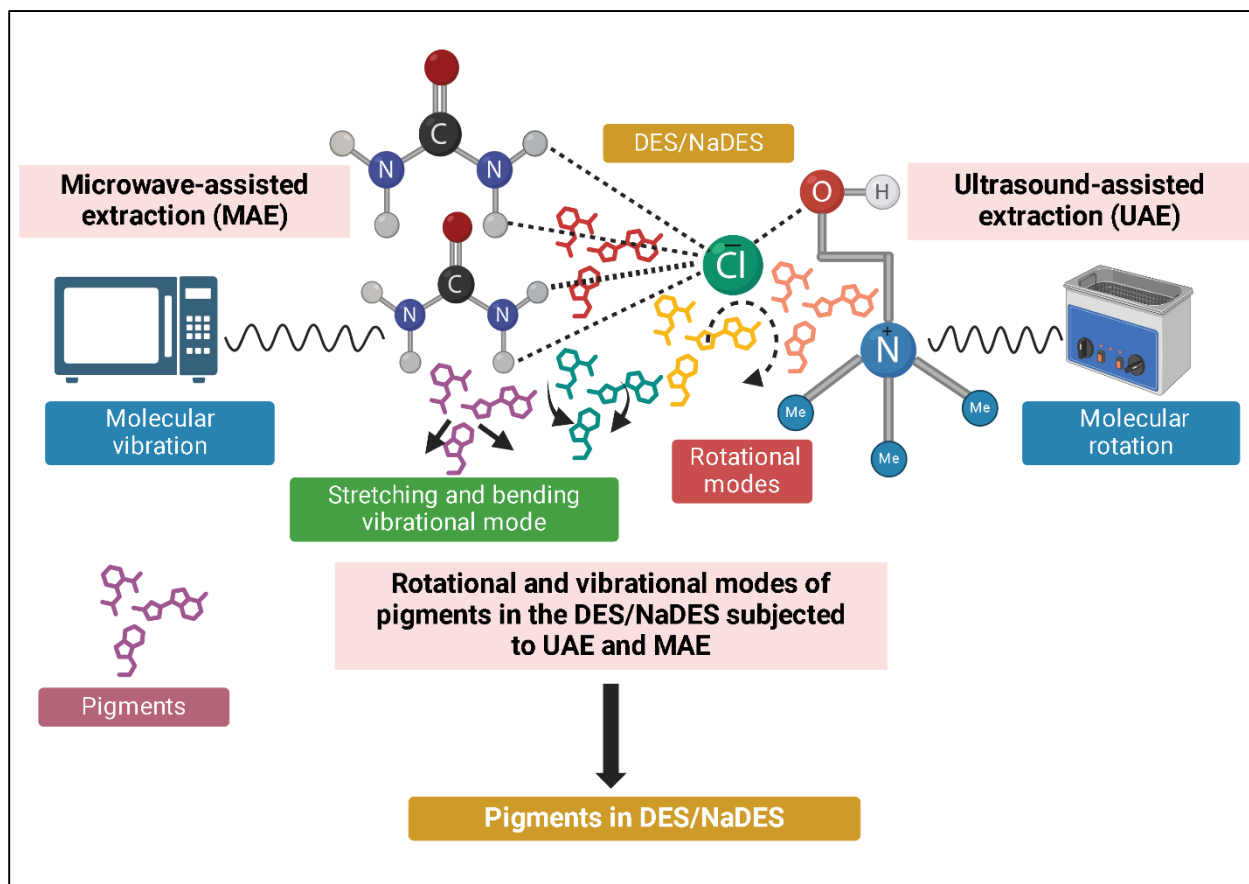


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1059 **Figure 1:** Schematic diagram of sources, extraction, and application of anthocyanins and

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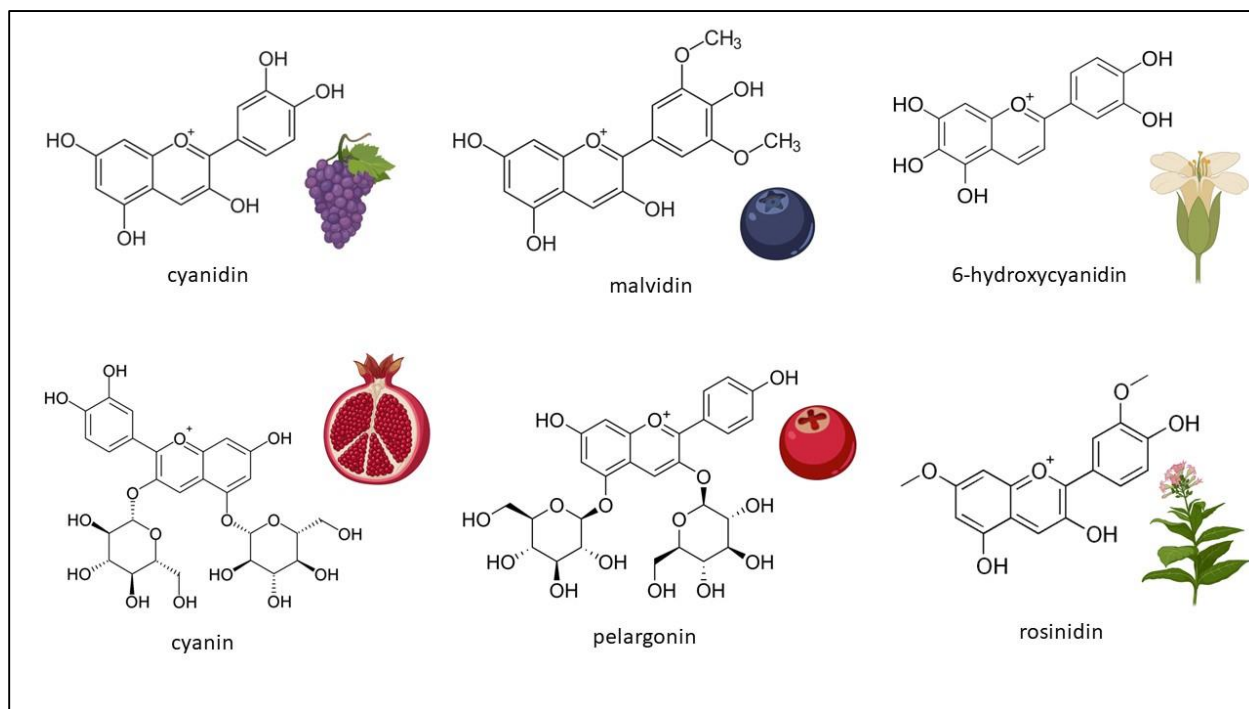
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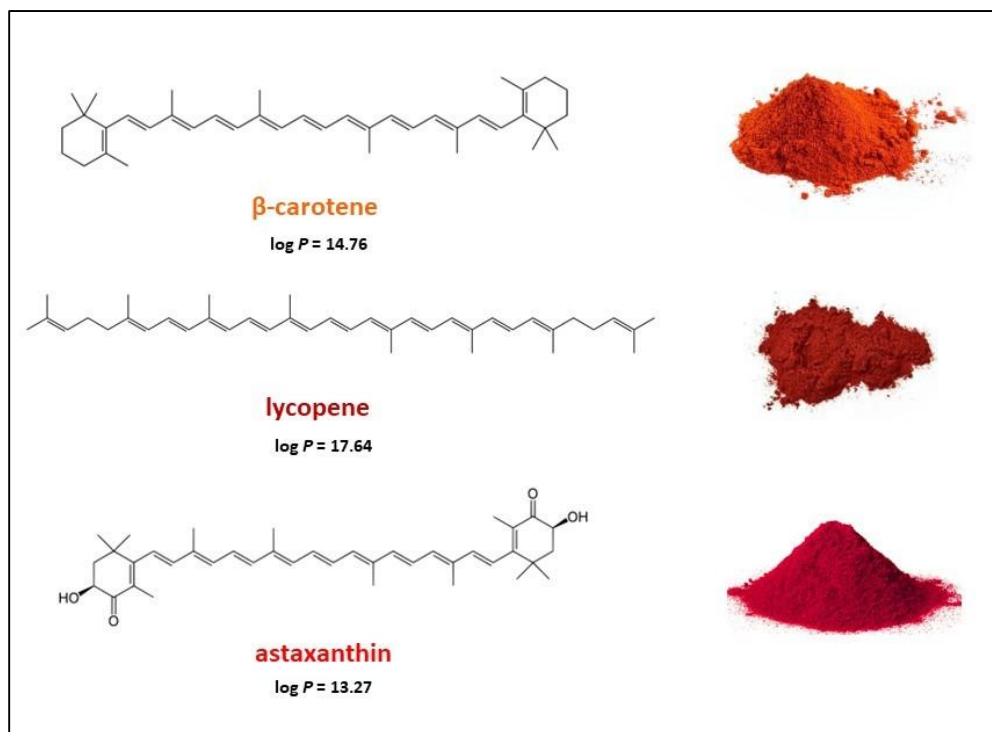
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1069 **Figure 3:** Chemical structure of selected anthocyanins with different functional groups and their
 1070 sources cyanidin from grapes, malvidin from blueberries and bilberries, 6-hydroxycyanidin from
 1071 borage, cyanin from pomegranate, pelargonin from cranberries, and rosinidin from roselle (created
 1072 using BioRender.com).



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1074 **Figure 4:** Chemical structure of main carotenoids with the corresponding powder representing

1075 the carotenoid extract in powdered form.

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1085 **List of abbreviation**

1086 DW: Dry weight

1087 FW: Fresh weight

1088 DS: Dry sample

1089 DES: Deep eutectic solvents

1090 NaDES: Natural deep eutectic solvents (NaDES)

1091 UAE: Ultrasound-Assisted Extraction

1092 MAE: Microwave-Assisted Extraction

1093 CGE: cyanidin-3-glucoside equivalents,

1094 D3G: delphinidin-3-sambubioside equivalents,

1095 MUAE: Microwave-Ultrasound-Assisted Extraction,

1096 PLE: Pressurized Liquid Extraction,

1097 HSH: High-speed homogenization

1098 CBE: Cavitation-burst extraction

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